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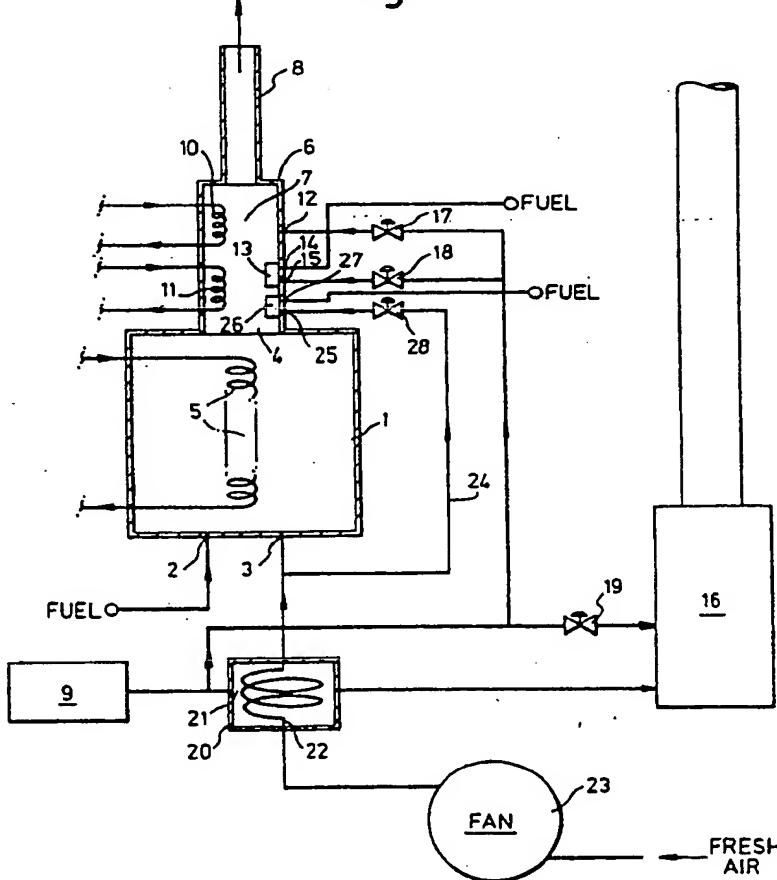
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(54) Utilising gas turbine exhaust in a chemical process plant

(57) In a chemical process plant, of the type having a gas turbine driven compressor and a fuel fired heater for heating a process medium, the exhaust from the gas turbine engine 9, is passed to a heat exchanger 20 and air at substantially atmospheric pressure and ambient temperature is forced through the heat exchanger by a fan 23 so as to be heated by the energy derived from the exhaust and is then fed to the radiant section 1 of the heater to support combustion therein. Gas turbine exhaust which has passed through the heat exchanger is subsequently exhausted to atmosphere via a stack 16. Air and any GTE which is surplus to the requirements of the radiant section 1, of the heater can be fed to a heat recovery convection section in the flue 7 of the heater where it can support further combustion (burners 26 and 13), thereby increasing flexibility of heat recovery in the convection section and in the overall operation of the heater.

Fig. 2.



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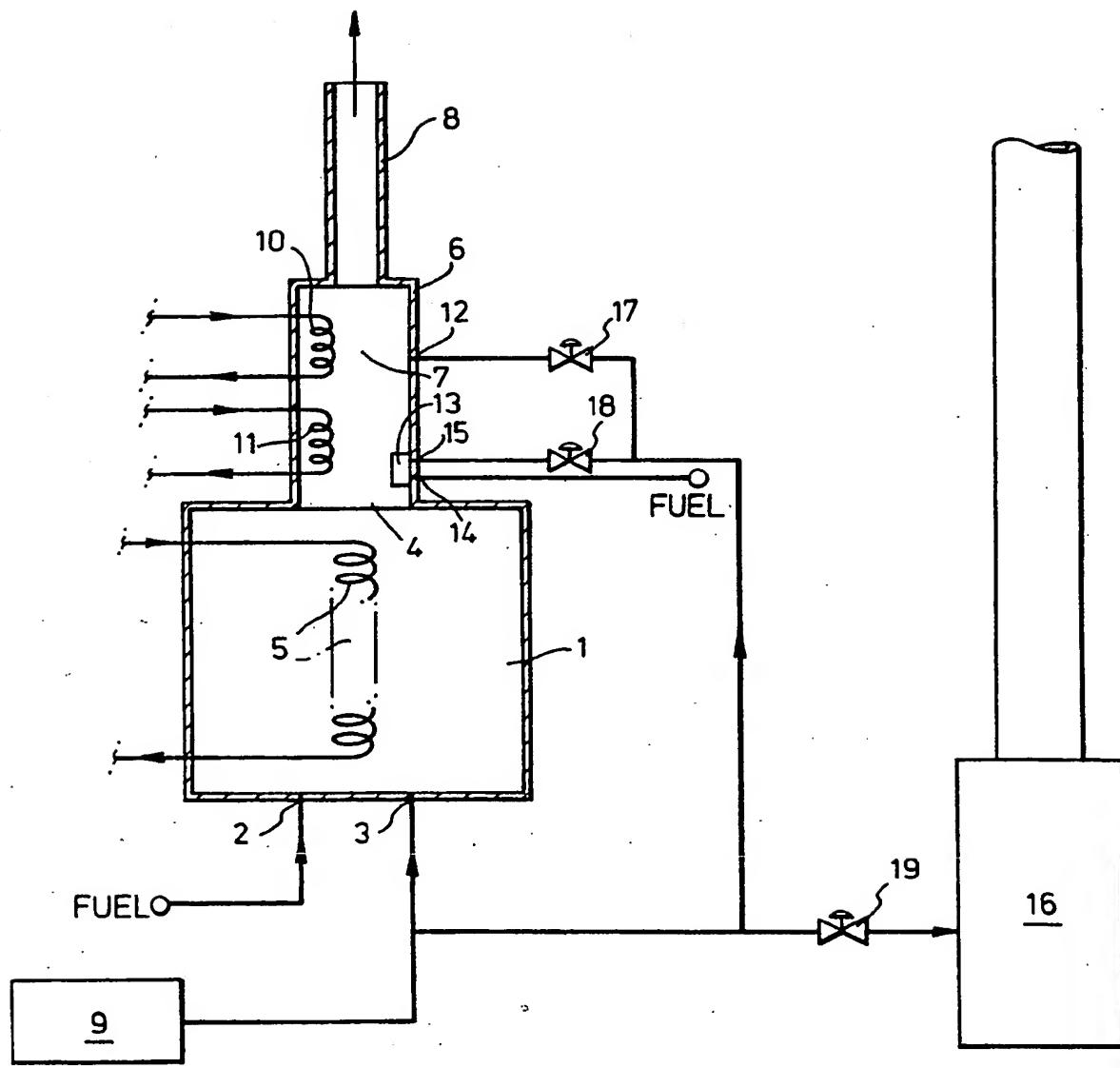


Fig. 1.

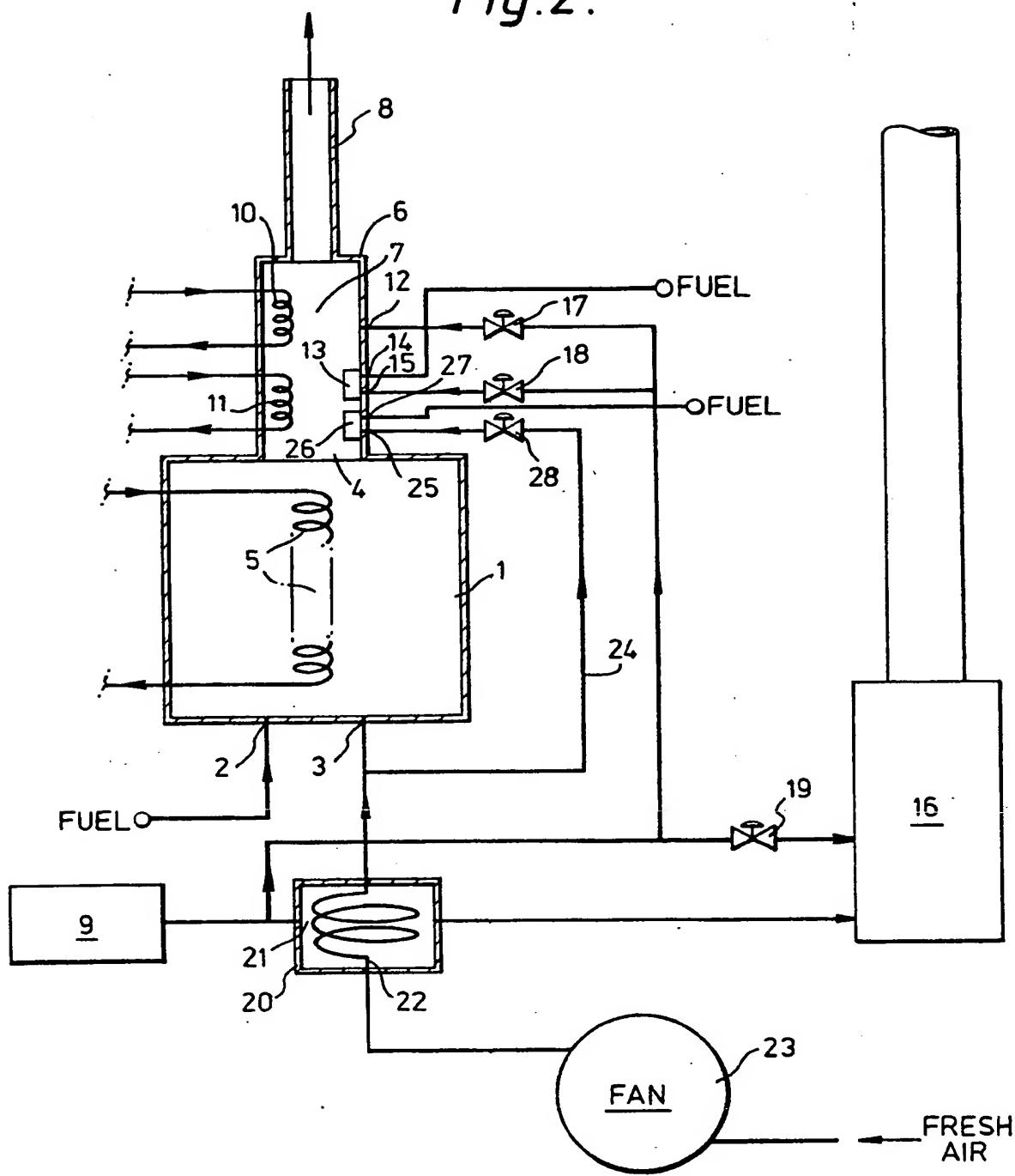
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Fig. 2.



SPECIFICATION

Improvements in chemical process fired heaters, furnaces or boilers

5 This invention relates to chemical process fired heaters, furnaces or boilers and to method of operation thereof.

In certain types of chemical process-plant

10 having gas or oil-fired heaters, furnaces or boilers having a radiant section, the heater fuel consumption is a function of the radiant section duty and the temperature of the flue gas as it leaves the radiant section is predetermined by the process, usually at some fixed value. To achieve a reasonable overall efficiency such plant usually incorporates a heat recovery convection section in which the flue gas leaving the radiant section is used to pre-

15 heat the process fluid which is to be supplied to the radiant section and to provide heat for the purposes of heating other process coils, for generating and super-heating steam and for heating steam generator feedwater coils.

20 Such plants as are here referred to conventionally use gas turbines to drive compressors and it is also a fairly common practice to utilize the gas turbine exhaust (GTE) as the source of oxygen for the combustion of the

25 fuel in the radiant section, i.e. as the oxidizing medium input thereto. Because GTE has typically an exhaust temperature of between 450°C to 550°C, by feeding GTE into the radiant section the fuel requirement of the heater

30 is reduced as compared with only using fresh air, even though the GTE contains only approximately 15 per cent oxygen by weight compared with approximately 23 per cent by weight for ambient air so that the quantity of

35 GTE required per unit input of fuel is greater than the quantity of fresh air alone required per unit input of fuel. Despite this increase the overall effect of utilizing GTE is to reduce the fuel consumption in the radiant section. Any

40 GTE which is surplus to that required in the radiant section can be used as an oxygen source for auxiliary firing within the convection banks or it can be dumped into the convection banks so that its sensible heat can be

45 recovered.

It is one object of the present invention to minimise fuel consumption in plant generally as described above by utilizing the GTE in a manner which is more efficient than has been

50 previously practised. It is also an object of the present invention to provide such plant modified in such a manner that in operation there is a substantial saving of fuel costs compared with previous practices. It is yet a further object of the invention to provide an increase in heat recovery flexibility.

These objects are achieved in accordance with the present invention by diverting the GTE from the heater input to at least one heat exchanger and by supplying the oxygen re-

quirement of the heater in the form of air which has passed through the at least one heat exchanger, said air being supplied to the heat exchanger as fresh air substantially at atmospheric pressure and ambient temperature by means of a forced draught or induced draught means. The GTE utilized in this manner which has passed through the heat exchanger is exhausted to atmosphere via an exhaust stack or, if so required, is utilized in some other manner. Any GTE which is surplus to the requirement of the heat exchanger is also exhausted directly to atmosphere or utilized as required in the heat recovery convection section or in other processes. Thus in the plant according to the invention there is provided a heat exchanger which on one side receives an input flow of air at substantially atmospheric pressure and ambient temperature and provides a supply of heated air to the normal oxidizing medium input of said radiant section and which on the other side receives an input in the form of exhaust gas from a gas turbine and outputs the exhaust gas after

55 it has given up sensible heat to the air flow to an exhaust means. It is to be understood that in the context of this statement the expression "radiant section" embraces heaters, furnaces and boilers used to implement chemical processes or to heat a medium used in such a process.

When some or all of the GTE leaving the gas turbine is passed through a heat exchanger and used to heat fresh air which is

60 then used by the radiant section burners, the fuel consumption of the heater can be further reduced compared with the use of GTE as described in prior processes. The fresh air can be heated to a temperature below that of the

65 GTE, and such temperature which may be approximately 50°C less than the GTE inlet temperature to the heat exchanger would depend on the investment criteria of the operator who would need to balance the capital invested in

70 the heat exchanger against the reduction in the running costs due to fuel savings. A temperature close to, say, 10°C lower than the GTE temperature would require a high investment in the heat exchanger with consequent

75 high fuel savings whereas a temperature difference between the heated fresh air and the GTE of, say, 200°C would lower investment cost but could not maximise fuel savings.

If surplus GTE is available a larger quantity

80 of fresh air than that required in the radiant section can be heated in the heat exchanger and then used as an oxygen source for auxiliary burners within the convection banks. Surplus GTE can also be used directly as an oxygen source for auxiliary firing within the convection banks or it can be dumped into the convection banks so that its sensible heat can be recovered.

The effect of this use of surplus GTE, in

85 addition to reducing fuel consumption, is to

increase the flexibility of heat recovery in the convection sections; i.e. the range of heat recovery duties, while still achieving a low flue gas exit temperature from the convection section

5 section, is greatly extended compared with the prior systems. Minimum heat recovery occurs when GTE surplus to that required for heating fresh air for the radiant section is dumped into the heat recovery convection section, at a point appropriate to its temperature level, without any auxiliary firing. Maximum heat recovery would occur when either all the GTE flows through the heat exchanger and the fresh air surplus to that required in the radiant

10 section is used as a source of oxygen for auxiliary firing within the heat recovery convection sections or when only some of the surplus GTE is passed through the heat exchanger to heat fresh air for auxiliary firing in

15 the convection sections with the remainder of the GTE dumped into the heat recovery convection sections at a point appropriate to its temperature level.

Any GTE surplus to that required in the heat exchanger, for heating fresh air, can be dumped direct to atmosphere or into any other heater convection section of the plant.

Hereinafter the invention is described by reference to a conventional plant and by way of example with reference to a modification of the conventional plant is illustrated in the accompanying drawings, wherein:-

Figure 1 illustrates a conventional plant commonly in use prior to this invention; and

35 Figure 2 illustrates a modification to the conventional plant to provide a plant according to this invention.

In Fig. 1 a conventional chemical process plant, used for example for cracking the hydrocarbons in a gas/steam mixture, has a heater comprising a radiant section chamber 1, a fuel input 2, an oxidizing medium input 3 and an exhaust gas output 5. The fuel is burnt within the radiant section chamber 1 using

40 gas turbine exhaust (GTE) as the oxidizing medium in such a manner as to maintain the temperature of the exhaust gas as it leaves the chamber at outlet 4 at a constant value. The process fluid is fed into a coil 5 at the

45 top of the chamber and leaves the coil 5 at the bottom of the chamber. A flue 6 includes a heat recovery convection section 7 and an exhaust stack 8. Inlet 3 receives its input from the exhaust of gas turbine 9 whose main

50 function is to drive a compressor (not shown).

The heat recovery convection section 7 in flue 6 which enables heat energy to be recovered from the flue gas before it is exhausted into the exhaust stack 8 comprises coils 10

55 and 11 containing heat recovery fluids (other coils may be incorporated to suit the requirements of the plant), a gas turbine exhaust input 12 and an auxiliary burner 13. The latter has a fuel input 14 and a gas turbine exhaust

60 input 15. Inputs 12 and 15 are coupled via

respective bypass ducts to the exhaust of the gas turbine 9 which is also connected by a further bypass duct to an auxiliary exhaust stack 16. Controllable valves 17, 18 and 19 in

70 the bypass ducts connected to the inputs 12 and 15 and to the auxiliary exhaust stack 16 are set by the operator or by him indirectly through a controller so as to control the flow of surplus GTE in the plant. Any exhaust from

75 the gas turbine 9 which is in excess of the requirement of the process section may be fed to the burner 13 or fed directly to the flue 7 so that is heat energy is also recovered in the convection banks of the heat recovery

80 convection section, or it may be exhausted directly to atmosphere via the auxiliary exhaust stack 16.

In the arrangement of Fig. 2 a two-channel heat exchanger 20 has its input-heat channel

85 connected to the exhaust of the gas turbine 9 and its output-heat channel 22 coupled to a supply of fresh air via a forced draught fan 23. After passing through the heat exchanger 20, the GTE is exhausted to atmosphere in an auxiliary exhaust stack 16. The fresh air in channel 23, now heated and remaining substantially at atmospheric pressure, is fed to the oxidizing medium input 3 of the radiant section chamber 1. Any GTE surplus to the

90 requirement of the heat exchanger 20 is treated in the same way as the surplus GTE in the prior art arrangement. Any heated air which is surplus to the requirements of combustion in the radiant section chamber 1 is

95 fed by duct 24 to the oxidizing medium input 25 of a further burner 26 having a fuel input 27. A controllable valve 28 in duct 24 is set by the plant operator, or indirectly by him through a controller, together with the valves

100 17, 18 and 19 in accordance with his operating criteria. By using air heated by the GTE to burn the fuel in the radiant section instead of directly using the GTE to burn the fuel a saving of fuel results during the operation of the

105 plant.

The use of the heat exchanger, in addition to providing the above-mentioned fuel saving, also provides enhanced flexibility of plant operation by virtue of the added heat recovery

115 facility, provided in the heat recovery convection section 7, comprising the burner 26 and the heated air supplied through duct 24 and controllable valve 28. By these means the operator may set up and control his plant for optimum performance with minimum fuel cost. The coils 10 and 11 can be used, as required, to preheat the process medium or mediums, to preheat boiler feedwater or to generate process steam, etc.

120 Various additional modifications may be made to the plant of Fig. 2, for example by adding heat recovery coils in the heat recovery convection section, or by using the GTE leaving the heat exchanger in yet further heating or heat recovery processes. Moreover,

an induced draught fan (not shown) may be used instead of the forced draught fan 23, or in addition to it, and be positioned between the air outlet of the heat exchanger 20 and

5 the inlet 3 of the radiant section. All such modifications should be considered as lying within the scope of the appended claims.

CLAIMS

10 1. A method of forming a chemical product by a heating process using a fuel fired heater wherein heated air for supporting combustion is supplied to a radiant section of the heater at substantially atmospheric pressure from a

15 heat exchanger which is supplied with fresh air and said heat exchanger receives a heat input in the form of exhaust gases from a gas turbine, the exhaust gases after passing through the heat exchanger being exhausted

20 to atmosphere.

2. A method of forming a chemical product according to Claim 1 wherein gaseous products of combustion are exhausted from the said radiant section at a temperature which is

25 predetermined by the process and a portion of the sensible heat in said gaseous products is subsequently recovered in a heat recovery section in the flue of the heater to which surplus GTE and/or surplus heated air from the

30 heat exchanger are also conducted so that the sensible heat therein is also recovered.

3. A method according to Claim 2 wherein said surplus GTE and said surplus air is used in respective burners in said flue as oxidizing

35 mediums for the combustion of additional fuel.

4. A method according to Claim 2 or Claim 3 wherein the flow of surplus GTE and the flow of surplus air to the heat recovery section are individually controllable.

40 5. A chemical process plant having a fuel fired radiant section for heating chemical process fluid wherein the oxidizing medium supplied to the radiant section for burning the fuel is air which has been heated in a heat ex-
45 changer, the latter being connected on its heat input side to the exhaust of a gas turbine so as to receive the exhaust gas therein, said air being supplied to the heat exchanger at ambient temperature and substantially at atmo-
50 spheric pressure.

55 6. A chemical process plant according to Claim 5 further comprising a heat recovery section to which surplus heated air from the heat exchanger is conducted so as to recover its sensible heat.

60 7. A chemical process plant according to Claim 6 wherein said recovery section includes at least one burner having a fuel input to which said surplus air is conducted for the purpose of supporting the combustion of fuel supplied to the burner.

65 8. A chemical process plant according to Claim 6 or Claim 7 wherein said recovery section also receives an input of GTE which is surplus to the requirement of the heat ex-

changer.

9. A chemical process plant incorporating a gas turbine, means for utilising the sensible heat of the gas turbine exhaust (GTE) and a

70 fuel-fired heater comprising a radiant section and a heat recovery section, fuel being burnt in said radiant section for the purpose of heating therein process-fluid contained in at least one process coil, said heat recovery section

75 being in the flue of the heater and containing one or more coils containing heat recovery fluids, characterised in that a first channel of a two-channel heat exchanger is connected between the gas turbine exhaust and an auxiliary

80 gas exhaust means and the second channel of the heat exchanger is connected between a source of fresh air and the fuel-oxidizing medium input of the said radiant section of the heater, said heat exchanger thereby supplying

85 heated fresh air to said radiant section at substantially atmospheric pressure.

10. A chemical process plant according to Claim 1 comprising a first burner in said flue and a bypass duct connected between the

90 output of the second channel of the heat exchanger and the first burner for conveying surplus heated air from the heat exchanger to the first burner for the purposes of supporting combustion therein, said first burner having a

95 further fuel supply.

11. A chemical process plant according to Claim 10 including a bypass duct connected between said gas turbine exhaust and said heat recovery section for conveying surplus

100 GTE to the latter.

12. A chemical process plant according to Claim 11 wherein said bypass duct between the gas turbine exhaust and the heat recovery section is coupled to a second burner situated

105 in the flue of the heater for supporting combustion in said burner, the latter having a fuel supply.

13. A chemical process plant according to Claim 12 further comprising controllable

110 means in said bypass ducts for controlling the passage of fluids therein.

14. A chemical process plant according to Claim 13 wherein said bypass duct between the gas turbine exhaust and the heat recovery

115 section has a branch coupled to the flue for bypassing said second burner and dumping GTE directly into the flue, said branch including a controllable means.

15. A chemical process plant according to Claim 9 to 14 wherein said source of fresh air includes a forced draught fan for forcing fresh air into the heat exchanger at substantially atmospheric pressure.

16. A chemical process plant according to any of Claims 9 to 15 including an induced draught fan situated between the fuel-oxidizing medium input of the radiant section and the heat exchanger.

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